cc:

Modeler

1050 17th Street, Suite 1700

Denver, CO 80265

July 2, 2015

D.E.

Wyoming Department of Environmental Quality Division of Air Quality

Herschler Building, 2E 122 West 25th Street

Cheyenne, Wyoming 82002

Subject: Mesa 8-17 Pad

Pinedale Field – Sublette County, Wyoming

Ladies/Gentlemen:

Tesoro Logistics – Rockies (TLLP), on behalf of QEPM Gathering I, LLC (QEPM), is submitting an application to modify/replace the dehydration unit equipment associated with the Mesa 8-17 Pad facility. The Mesa 8-17 dehydration equipment is owned by OEPM, but the production equipment is owned and operated by QEP Energy Company (QEPE). The Mesa 8-17 Pad is located in the SENE of Section 17, T32N, R109W in Sublette County, Wyoming.

An application was recently submitted to account for the split of the original OEPE permit into a permit for the QEPM dehydration equipment and the QEPE production equipment. This application is intended to obtain a modified permit to account for the replacement of the historic 40 MMSCFD dehydration unit with a 10 MMSCFD dehydration unit. In addition to the replacement of the dehydration unit, the line heater and associated heat trace pump have been removed.

The produced natural gas flows from all wells at this location through QEPE-owned production equipment and into a QEPM-owned dehydration unit separator and TEG dehydration unit. The emissions for the dehydration unit are controlled by a QEPM-owned BTEX combustor.

Based on the use of dehydration unit control and the federally enforceable limits provided by the Division's permitting process, the dehydration unit associated with this facility is a "synthetic minor" with respect to the National Emissions Standards for Hazardous Air Pollutants from Oil and Gas Natural Gas Production Facilities 40 CFR Part 63 Subpart HH. This unit is exempt from control requirements of 40 CFR 63.764(d) because the average emissions of benzene are less than 0.90 megagrams per year (40 CFR 63.764(e)(2)).

OEPE has implemented an infrared (IR) Leak Detection and Repair (LDAR) program as BACT for fugitive emission sources at the Mesa 8-17 Pad facility. QEPE has agreed to inspect QEPM equipment at this location with a FLIR camera as part of QEPE's ongoing LDAR program. As per WDEQ guidance, contributions from fugitive emission sources can be treated as insignificant at pads where an IR LDAR program has been implemented. Therefore, both historical and current fugitive emissions at the Mesa 8-17 Pad are deemed insignificant.

Under Attachment A of this submittal, the required WAQD IMPACT forms are included. Attachment B includes all supporting emissions calculations for the QEPM emissions at the Mesa 8-17 Pad.

To ensure offsets are not being double counted and credits are available for future permitting actions, the Division has requested that a spreadsheet be developed to track all permitting actions since April 1, 2008. This QEPM offset tracking spreadsheet has been recently created due to an equipment split at multiple facilities owned by QEPE with QEPM dehydration units on location. The offset tracking spreadsheet has been revised in this submittal to show both current QEPM emissions as well as QEPM's historical contribution of emissions at the Mesa 8-17 Pad. This spreadsheet is included under Attachment C.

If you should have any questions or need additional information in support of this submittal, please contact me at (303) 640-4238 or Lesair Environmental at (303) 904-2525.

Sincerely,

Daniel Pring

Senior Environmental Air Engineer

Enclosures

cc: Lesair Environmental

Company Name: **QEPM Gathering I, LLC**

Facility Name: Mesa 8-17

Attachment A

WAQD IMPACT Forms

WYOMING

Department of Environmental Quality Air Quality Division

Permit Application Form

-	Is this a revision to an exist	ing application?		
WYOMING	is this a revision to an exist	ing application.		
	Yes X	No	Date of A	pplication: 7/6/2015
	Previous Application #:	Pending		
COMPANY INFO	RMATION:		•	
Company Name:		QEPM Gathe	ring I. LLC	
Address:	105	50 17th Street, Suite 170		
City: Den	ver State:	СО		Zip Code: 80265
Country:	USA	Phone Number:	303-640-	4238
FACILITY INFORM	//ATION:			
Facility Name:		Mesa 8	-17	
New Facility or Existin	g Facility: Existing			
Facility Description:	Multi-	well production facility	with one dehydration uni	t
Facility Class:	Synthetic Minor	Operating Status:		
Facility Type:	Production Site			
For Oil & Gas Product	tion Sites ONLY:			
First Date of Producti	on (FDOP)/Date of Modific	ation: 12/07/2001	/ 05/07/2015	
Does production at th	nis facility contain H2S?*	NO		
*If yes, contact the D	ivision.			
API Number(s):				
		49-035-22648, 2	5522, 25524, 25525,	
	25523,2552	6,25516,25536,25517,2	5518,25519,25520,25521	,25645,25644
NAICS Code:		2	1111	
FACILITY LOCATION	ON:			
*Enter the facility location	on in either the latitude/longitu	ide area or section/townsh	ip/range area. Both are not	equired.
Physical Address:				
City:		Zip Code:		
State:	County:			
OR				
Latitude: 42.74	1889 Longitude:	109.85027		
Quarter Quarter:	SE Longitude.	Quarter:	NE	
Section: 17		32N	IVL	Range: 109W
- X - X - X - X - X - X - X - X - X - X	and latitude, use NAD 83/W		ts after the decimal (i e .A	
CONTACT INFOR		0304 datam ana 3 digi	is after the accimal file. 4	1.12545, -107.50705)
A 100				
	AND NSR Permitting Contact is requi			
Title: Mr.	First Name:		Daniel	
Last Name:	Pring			
Company Name:		QEPM Gathe		
Job Title:		enior Environmental Ai		
Address:		1050 17th Street, Suit		
	Denver	State:	СО	
Zip Code: 80265	200 445		3220000 .	
Primary Phone No.:	303-640-4238	E-mail:		ng@tsocorp.com
Mobile Phone No.:		Fax No.:		
Contact Type:	Compliance	Start Date:	Jun-15	

Additional Contact Type (if needed):	
Title: First Name:	
Last Name:	
Company Name:	
Job Title:	
Address:	
City: State:	
Zip Code:	
Primary Phone No.: E-mail:	
Mobile Phone No.: Fax No.:	
Contact Type: Start Date:	
FACILITY APPLICATION INFORMATION:	
General Info:	
	N
Has the facility changed location or is it a new/ greenfield facility?	No
Has a Land Use Planning document been included in this application?	No
Is the facility located in a sage grouse core area?*	No
If the facility is in a sage grouse core area, what is the WER number?	NA
* For questions about sage grouse core area, contact WY Game & Fish Department.	
Federal Rules Applicability - Facility Level:	
Prevention of Significant Deterioration (PSD):	No
Non-Attainment New Source Review:	No
Modeling Section:	
Has the Air Quality Division been contacted to determine if modeling is required?	No
Is a modeling analysis part of this application?	No
Is the proposed project subject to Prevention of Significant Deterioration (PSD) requirements?	No
Has the Air Quality Division been notified to schedule a pre-application meeting?	No
Has a modeling protocol been submitted to and approved by the Air Quality Division?	No
Has the Air Quality Division received a Q/D analysis to submit to the respective FLMs to	
determine the need for an AQRV analysis?	No
Required Attachments:	
_	
Facility Map Process Flow Diagram	
Modeling Analysis (if applicable)	
Land Use Planning Document	
Detailed Project Description Emissions Calculations	
Emissions Calculations	
Michael D. Caldanda	
	oro Logistics- Rockies
Responsible Official (Printed Name)	itle
an Official Representative of the Company, state that I have knowledge of the facts herein set for	
are true and correct to the best of my knowledge and belief. I further certify that the operation	
and emission rates listed on this application reflect the anticipated emissions due to the operation	3
facility will operate in compliance with all applicable Wyoming Air Quality Standards and Regula	tions.
	-11
19 1) 1/44	7/3/15
Signature: Dat	e:
(ink)	

Dehydration Unit

Company Equipment ID:	
Company Equipment Description:	(1) 10 MMSCFD TEG Dehydration Unit
	· · · · · · · · · · · · · · · · · · ·
Operating Status: Operating	
Initial Construction Commencement Date:	5/7/2015
Initial Operation Commencement Date:	5/7/2015
Most Recent Construction/ Modification	
Commencement Date:	5/7/2015
Most Recent Operation Commencement Da	te: 5/7/2015
Select reason(s) for this emissions unit bein	g included in this application (must be completed regardless of date of
installation or modification):	
Reason: Modification	
If reason is <i>Reconstruction</i> or <i>Temporary Polymers</i>	ermit or Other, please explain below:
Production equipment has been changed at	this facility, therefore this source has been modified
Dehydration Type: TEG	Design Capacity (MMscf/day): 10
Temperature of Wet Gas (F):	79
Water Content of Dry Gas (lbs H2O/MMscf)	: 5
Pressure of Wet Gas (psig): 4	79
Manufacturer Name of Glycol Circulation Pu	ımp: Kimray
Model Name and Number of Glycol Circulat	ion Pump: (1) Kimray 9015 PV
Water Content of Wet Gas (lbs H2O/MMscf	54.47
Flow Rate of Dry Gas (MMscfd): 8	.0
Type of Glycol Circulation Pump:	as
Pump Volume Ratio (acfm/gpm):	0.08
Actual LEAN Glycol Circulation Rate (gpm):	1.5
Maximum LEAN Glycol Circulation Rate (gpn	n):1.5
Source of Motive Gas for Pump:	ield Gas
Include Glycol Flash Separator?:	es
Flash Tank Off Gas Stream (scf/hr):	293
Flash Tank Operating Temperature (F):	100
Flash Tank Operating Pressure (psig):	35
	ombustor
Is Vessel Heated?: No	
Additional Gas Stripping?:	
	<u>A</u>
Source of Stripping Gas:	<u>A</u>
SCC Codes: List all Source Classification Cod (e.g., 1-02-002-04).	de(s) (SCC) that describe the process(es) performed by the emission source
	3-10-003-01
Potential Operating Schedule: P	rovide the operating schedule for this emission unit.
12/20/20/20/20/20/20/20/20/20/20/20/20/20	**************************************
	760
i iours/year. o	700

Control Equipment: Yes
If yes, please fill out and attach the appropriate Control Device and Release Point Information worksheets.
Best Available Control Technology (BACT): Was a BACT Analysis completed for this emission unit?
☐ Yes ☑ No
Pollutant:
Proposed BACT: NA - JPAD/UGRB requires combustor at startup
*If yes, attach BACT Analysis with this application.
Lowest Achievable Emission Rate (LAER): Was a LAER Analysis completed for this emission unit?
☐ Yes ✓ No
Pollutant:
Proposed LAER:
*If yes, attach LAER Analysis with this application.
Federal and State Rule Applicability:
New Source Performance Standards (NSPS): Not Affected
New Source Performance Standard are listed under 40 CFR 60- Standards of
Performance for New Stationary Sources.
NSPS Subpart:
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61): Not Affected
National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR 61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride). Part 61 NESHAP Subpart:
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63): Subject, But Exempt
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63) standards are listed under 40 CFR 63
Part 63 NESHAP Subpart: HH
Prevention of Significant Deterioration (PSD): Not Affected
These rules are found under WAQSR Chapter 6, Section 4.
Non-Attainment New Source Review: Not Affected
These rules are found under WAQSR Chapter 6, Section 13.

Control Equipment:

Condenser

Manufacturer:	Pesco					Date Insta	lled:	5/7/20	15	
Model Name and						Company	Control			
Number:	N/A					Equipmen	t ID:	N/A		
Company Control Equi	ipment									
Description:		(1) 10 MM	SCFD TE	G D	ehydration	Unit Reboi	ler Still Ven	t Conde	nser	
Pollutant(s) Controlled	d:	СО	□ NO:	x	Pb	SO2	✓ VOC	□ PM		
PM (FIL)	□ РМ С	ondensible	□ P	M 10) (FIL)	☐ PM 2	.5 (FIL)	☐ PM	1 10 🔲	PM 2.5
✓ Other HAPS										
						_				
Design Control Efficier	ncy (%):				Capture Ef	ficiency (%)	:	100		
Operating Control Effi	ciency (%):									
Condenser Type:	Indirect Co	ntact				_				
Coolant Type:	Produced (Gas								
Design Coolant Temp.	Range (F):									
Design Coolant Flow R	ate (gpm):						-			
Max. Exhaust Gas Tem	np (F):	95				Inlet Gas F	low Rate (a	cfm):		13.45
Outlet Gas Flow Rate ((acfm):	0.159				Inlet Gas T	emp (F):	212		
Operating Pressure (p	sia):	12				Outlet Gas	Temp (F):	95		
☐ This is the	only contro	l equipmen	t on this	s air	contamina	nt source				
If not, this control equ	ipment is:			Prim	nary	✓ Seco	ndary		Parallel	
List all other emission	units that a	re also								
vented to this control	equipment	:	None							
List all release point ID	s associate	d with this								
control equipment:			N/A							

Flare

Company Equipment ID:				
Company Equipment Description:	BTEX Comb	ustor		
Operating Status: Operating				
Initial Construction Commencement D	Date:	12/7/2001		_
Initial Operation Commencement Dat	e:	12/7/2001		_
Most Recent Construction/ Modificati	on			
Commencement Date:		5/7/2015		_
Most Posent Operation Commonsor	out Date:	F /7 /201F		
Most Recent Operation Commenceme		5/7/2015	. h	_
Select reason(s) for this emissions un	it being included in th	is application (must	be complete	ed regardless of date
of installation or modification):				
Reason: Modificatio	n			
If reason is <i>Reconstruction</i> or <i>Tempor</i>	rary Permit or Other,	please explain belov	w:	
Maximum Design Capacity (MMSCF/h Minimum Design Capacity (MMSCF/hi Pilot Gas Volume (scf/min):				
Emergency Flare Only: No		Ignition Device Type	2:	Pilot
Btu Content (Btu/scf): 1079.66		Smokele	ss Design:	Yes
Assist Gas Utilized? No	Continuous	ly Monitored?	Yes	
Waste Gas Volume: 7206		Units:	scf/day	
Installation Date: 12/7/2001				_
SCC Codes: List all Source Classification source (e.g., 1-02-002-04).	on Code(s) (SCC) that		s(es) perform	ned by the emission
Potential Operating Schedule:	Provide the operating	schedule for this em	ission unit.	
t with the second	24			
Hours/year: 8760				
_				

Control Equipment: NA
If yes, please fill out and attach the appropriate Control Device and Release Point Information worksheets.
Best Available Control Technology (BACT): Was a BACT Analysis completed for this emission unit? Yes No Pollutant: Proposed BACT:
*If yes, attach BACT Analysis with this application.
n yes, attach sher maysis with this application.
Lowest Achievable Emission Rate (LAER): Was a LAER Analysis completed for this emission unit? Yes No Pollutant:
Proposed LAER:
*If yes, attach LAER Analysis with this application.
Federal and State Rule Applicability: New Source Performance Standards (NSPS): New Source Performance Standard are listed under 40 CFR 60- Standards of Performance for New Stationary Sources. NSPS Subpart:
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61): National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR 61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride). Part 61 NESHAP Subpart:
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63): National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63) standards are listed under 40 CFR 63
Part 63 NESHAP Subpart: HH
Prevention of Significant Deterioration (PSD): Not Affected These rules are found under WAQSR Chapter 6, Section 4.
Non-Attainment New Source Review: Not Affected These rules are found under WAQSR Chapter 6. Section 13

Control Equipment:

Flare/Combustor

Manufacturer:	Cimarron			Date Installed:	5	5/7/2015
Model Name and				Company Contro	- -	
Number:	BTEX			Equipment ID:	N	I/A
Company Control Equ	ipment					
Description:		BTEX Comb	bustor associated with	10 MMSCFD TEG	Dehyd	ration Unit
Pollutant(s) Controlled	d:	СО	□ NOx □ Pb	□SO2 ✓	VOC [PM
PM (FIL)	□ РМ С	ondensible	☐ PM 10 (FIL)	☐ PM 2.5 (FIL)] [☐ PM 10 ☐ PM 2.5
✓ Other HAPS						
Design Control Efficier	ncy (%):	98	Capture E	fficiency (%):	_1	.00
Operating Control Effi	ciency (%):		98	_		
Flare Type:	Enclosed		Elevated F	lare Type:	N/A	A
Ignition Device:	Yes		Flame Presence Sense	or: Yes		
Inlet Gas Temp (F):	95		Flame Pre	sence Type:		Thermocouple
Gas Flow Rate (acfm):		6.	59	Outlet Gas Temp	(F):	
✓ This is the	only control	equipmen	t on this air contamina	ant source		
If not, this control equ	ipment is:		Primary	Secondary		Parallel
List all other emission	units that a	re also				
vented to this control	equipment:		10 MMSCFD TEG Deh	ydration Unit w/ (Conden	ser and Flash Tank
List all release point II	Os associate	d with this		-		
control equipment:						

Heater/Chiller

Company Equipment II	D:					
Company Equipment D	(1	1) 0.125 MMB	tu/hr TEG Reboi	ler		
0 1' 6' 1	To					
Operating Status:	Operating					
Initial Construction Cor				5/7/2015		_
Initial Operation Comm				5/7/2015		_
Most Recent Construct		cation				
Commencement Date:		_		5/7/2015		_
Most Recent Operation	n Commenc	ement				
Date:				5/7/2015	W.	_
Select reason(s) for thi	is emission:	s unit being in	cluded in this	application (mu	ıst be compl	eted regardless of
date of installation or	modificatio	n):				
Reason	Modificati	on				
If reason is <i>Reconstruct</i> New wells and product						e has been modified
				,,		
Firing Type:	Direct	1				
Heat Input Rating:	0.125	_		Units:	MMBtu/h	nr
Primary Fuel Type:	Field Gas		``			<u></u>
Secondary Fuel Type:	N/A					
Heat Content of Fuel:	1080				Units:	BTU/scf
Fuel Sulfur Content:	N/A			Units:	O TITLES.	510/301
r der odri di contenti.	14//			omes.		_
SCC Codes: List all Sou source (e.g., 1-02-002-		cation Code(s)	(SCC) that d	escribe the proc	ess(es) perfo	ormed by the emission
			3-10-002-2	7		
Potential Operating So	chedule:	Provide the c	perating sche	edule for this em	ission unit.	
Hours/day:		24				
Hours/year	:	8760				

Control Equipment: N/A If yes, please fill out and attach the appropriate Control Device and Release Point Information worksheets.	
Best Available Control Technology (BACT): Was a BACT Analysis completed for this emission unit? Yes No Pollutant: Proposed BACT:	
*If yes, attach BACT Analysis with this application.	_
Lowest Achievable Emission Rate (LAER): Was a LAER Analysis completed for this emission unit? Yes No Pollutant: Proposed LAER: *If yes, attach LAER Analysis with this application.	_
Federal and State Rule Applicability: New Source Performance Standards (NSPS): New Source Performance Standard are listed under 40 CFR 60- Standards of Performance for New Stationary Sources. NSPS Subpart:	
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61): Not Affected	
National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR 61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride). Part 61 NESHAP Subpart:	_
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63): Not Affected	
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63) standards are listed under 40 CFR 63 Part 63 NESHAP Subpart:	
Prevention of Significant Deterioration (PSD): Not Affected These rules are found under WAQSR Chapter 6, Section 4.	
Non-Attainment New Source Review: Not Affected These rules are found under WAQSR Chapter 6, Section 13.	

Pneumatic Equipment (Pumps and Controllers)

Company Equipment ID:						
Company Equipment Description:						
(4) Cemco/W	ellmark Mizer Low-Bleed Pneuma	tic Liquid Level Control	ler(s)			
Operating Status: Operating						
Initial Construction Commencemen	nt Date: 5/7/	/2015				
Initial Operation Commencement I	Date: 5/7/	/2015	-			
Most Recent Construction/ Modifie	cation		-			
Commencement Date:	5/7/	/2015				
Most Recent Operation Commence	ement		-			
Date:	5/7/	/2015				
Select reason(s) for this emissions	unit being included in this application	ation (must be comple	eted regardless of date of			
installation or modification):		_				
Reason: Modification	า]				
If reason is <i>Reconstruction</i> or <i>Tem</i> New wells and production equipments			e has been modified			
Type of Equipment: Controller Motive Force: Field Gas		VOC Content (%):	6.30%			
HAP Content (%): 0.25%						
SCC Codes: List all Source Classification Code(s) (SCC) that describe the process(es) performed by the emission source (e.g., 1-02-002-04).						
	3-10-002-99					
Hours/day:	Provide the operating schedule for	this emission unit.				
Hours/year: 8	3760	-				

Control Equipment: No
If yes, please fill out and attach the appropriate Control Device and Release Point Information worksheets.
Best Available Control Technology (BACT): Was a BACT Analysis completed for this emission unit?
☐ Yes ☑ No
Pollutant:
Proposed BACT:
*If yes, attach BACT Analysis with this application.
Lowest Achievable Emission Rate (LAER): Was a LAER Analysis completed for this emission unit?
☐ Yes ✓ No
Pollutant:
Proposed LAER:
*If yes, attach LAER Analysis with this application.
Federal and State Rule Applicability:
New Source Performance Standards (NSPS): Not Affected
New Source Performance Standard are listed under 40 CFR 60-
Standards of Performance for New Stationary Sources.
NSPS Subpart:
National Emission Standards for Hazardous Air Pollutants (NESHAD Port C1).
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61): Not Affected
National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR 61.
(These include asbestos, benzene, beryllium, mercury, and vinyl chloride).
Part 61 NESHAP Subpart:
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63): Not Affected
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63) standards are listed under 40 CFR 63
Part 63 NESHAP Subpart:
rait os Nesilar subpait.
Prevention of Significant Deterioration (PSD): Not Affected
These rules are found under WAQSR Chapter 6, Section 4.
,
Non-Attainment New Source Review: Not Affected
These rules are found under WAQSR Chapter 6, Section 13.

Separator/Treater

Company Equipment ID:		
Company Equipment Description	on:	(1) Dehy Unit Separator
Operating Status: Operatin	ıg	
Initial Construction Commence	ment Date:	5/7/2015
Initial Operation Commenceme	ent Date:	5/7/2015
Most Recent Construction/ Mo	dification	
Commencement Date:		5/7/2015
Most Recent Operation Comme	encement	
Date:		5/7/2015
Select reason(s) for this emissi	ons unit being	included in this application (must be completed regardless of date
of installation or modification)):	
Reason: Modifica	ition	
		een added to this facility, therefore this source has been modified
Type of Vessel: 3-Pha	se Separator	Is Vessel Heated? No
Operating Temperature (F):	79	
Operating Pressure (psig):	479	
SCC Codes: List all Source Clas source (e.g., 1-02-002-04).	sification Code	e(s) (SCC) that describe the process(es) performed by the emission
		3-10-001-07
Potential Operating Schedule: Hours/day: Hours/year:	Provide the 24 8760	e operating schedule for this emission unit.

Control Equipment: N/A
If yes, please fill out and attach the appropriate Control Device and Release Point Information worksheets.
Best Available Control Technology (BACT): Was a BACT Analysis completed for this emission unit?
☐ Yes ✓ No
Pollutant:
Proposed BACT:
*If yes, attach BACT Analysis with this application.
Lowest Achievable Emission Rate (LAER): Was a LAER Analysis completed for this emission unit?
☐ Yes ✓ No
Pollutant:
Proposed LAER:
*If yes, attach LAER Analysis with this application.
Federal and State Rule Applicability:
New Source Performance Standards (NSPS): Not Affected
New Source Performance Standard are listed under 40 CFR 60-
Standards of Performance for New Stationary Sources.
NSPS Subpart:
National Enviroing Chandenda for Hannahava Air Delly touts (NECHAD Dayle Cd.)
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61): Not Affected
National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CF
61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride).
Part 61 NESHAP Subpart:
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63): Not Affected
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63)
standards are listed under 40 CFR 63
Part 63 NESHAP Subpart:
•
Prevention of Significant Deterioration (PSD): Not Affected
These rules are found under WAQSR Chapter 6, Section 4.
Non-Attainment New Source Review: Not Affected
These rules are found under WAQSR Chapter 6, Section 13.

Storage Tank/Silo

Company Equipment ID:					
Company Equipment Description:	(1) 300 b	bl Test Tank			
Operating Status: Operating					
Initial Construction Commenceme	ent Date:	12/7	7/2001		_
Initial Operation Commencement	Date:	12/7	7/2001		
Most Recent Construction/ Modif	ication				_
Commencement Date:		5/7	/2015		_
Most Recent Operation Commend	cement				_
Date:		5/7	/2015		
Select reason(s) for this emission	s unit being included i	n this applic	cation (mus	t be comple	eted regardless of date
of installation or modification):			_		
Reason: Modification	on				
If reason is <i>Reconstruction</i> or <i>Ter</i>	nporary Permit or Oth	er, please e	explain belo	w:	
Production equipment has been of	changed, therefore this	source has	been modif	ied	
Material Type: Liquid					
Description of Material Stored:	oil/produ	iced water o	only during	periods of w	vell testing
			T		
Capacity: 300		Units:	barrels	_	
Maximum Throughput:	NA		_	Units:	
Maximum Hourly Throughput:	NA		_	Units:	
Is Tank Heated?: Yes					
SCC Codes: List all Source Classif	ication Code(s) (SCC)	that describe	e the proces	ss(es) perfo	rmed by the emission
source (e.g., 1-02-002-04).					
	3-10-	002-99			
Potential Operating Schedule:	Provide the operating	schedule for	r this emissi	ion unit.	
Hours/day:	intermittent		_		
Hours/year:	intermittent		_		

Control Equipment: No
If yes, please fill out and attach the appropriate Control Device and Release Point Information worksheets.
Best Available Control Technology (BACT): Was a BACT Analysis completed for this emission unit?
☐ Yes ✓ No
Pollutant:
Proposed BACT:
*If yes, attach BACT Analysis with this application.
Lowest Achievable Emission Rate (LAER): Was a LAER Analysis completed for this emission unit?
☐ Yes ✓ No
Pollutant:
Proposed LAER:
*If yes, attach LAER Analysis with this application.
Federal and State Rule Applicability:
New Source Performance Standards (NSPS): Not Affected
New Source Performance Standard are listed under 40 CFR 60-
Standards of Performance for New Stationary Sources.
NSPS Subpart:
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61): Not Affected
National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR
61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride).
Part 61 NESHAP Subpart:
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63): Not Affected
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63) standards are listed under 40 CFR 63
Part 63 NESHAP Subpart:
Tute 05 NESTING Subpare.
Prevention of Significant Deterioration (PSD): Not Affected
These rules are found under WAQSR Chapter 6, Section 4.
Non-Attainment New Source Review: Not Affected
These rules are found under WAQSR Chapter 6, Section 13.

Fugitives

Company Equipment ID: Facility-V	/ide Fugitive Emissions
Company Equipment Description:	[(1) Dehy Separator, (1) Test Tank, (1) Dehy w/ Combustor]
50 pt 0300 1000	
Operating Status: Operating	
Initial Construction Commencement Date:	12/7/2001
Initial Operation Commencement Date:	12/7/2001
Most Recent Construction/ Modification	
Commencement Date:	5/7/2015
Most Recent Operation Commencement	
Date:	5/7/2015
Select reason(s) for this emissions unit bei	ng included in this application (must be completed regardless of date of
installation or modification):	
Reason: Equipment replaced	
If reason is <i>Reconstruction</i> or <i>Temporary I</i> Production equipme	Permit or Other, please explain below: Int has been changed, therefore this source has been modified
Type of Fugitive Emission: Fugitive I	eaks at O&G
SCC Codes: List all Source Classification Co 02-002-04).	ide(s) (SCC) that describe the process(es) performed by the emission source (e.g., 1-
3-10-	002-07, 3-10-002-23, 3-10-002-24, 3-10-002-26
Potential Operating Schedule: Provide to the Hours/day: 24 8760	he operating schedule for this emission unit.

Control Equipment: Yes	
If yes, please fill out and attach the appropriate Control Device and Release Point Inform	ation worksheets.
Best Available Control Technology (BACT): Was a BACT Analysis completed for this emiss	sion unit?
✓ Yes	
Pollutant:	
Proposed BACT: Facility-wide LDAR using FLIR Infrared Camera (as per QEPE LDAR Pr	otocol)
*If yes, attach BACT Analysis with this application.	
Lowest Achievable Emission Rate (LAER): Was a LAER Analysis completed for this emission	on unit?
☐ Yes ✓ No	
Pollutant:	
Proposed LAER:	
*If yes, attach LAER Analysis with this application.	
Federal and State Rule Applicability:	
New Source Performance Standards (NSPS): Not Affected	
New Source Performance Standard are listed under 40 CFR 60-	
Standards of Performance for New Stationary Sources.	
NSPS Subpart:	
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61):	Not Affected
National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) a	are listed under 40 CFR 61. (These
include asbestos, benzene, beryllium, mercury, and vinyl chloride).	
Part 61 NESHAP Subpart:	
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63):	Not Affected
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63)	
standards are listed under 40 CFR 63	
Part 63 NESHAP Subpart:	
Prevention of Significant Deterioration (PSD): Not Affected	_
These rules are found under WAQSR Chapter 6, Section 4.	
New Attainment New Course Projects	
Non-Attainment New Source Review: Not Affected Those rates are found under WA OCR Observer C. Continue 12	
These rules are found under WAQSR Chapter 6, Section 13.	

Company Name: QEPM Gathering I, LLC

Facility Name: Mesa 8-17

Attachment B

Supporting Emissions Calculations

Process Description

This is the process description associated with the dehydration equipment (owned by QEPM Gathering I, LLC) which is co-located with Mesa 8-17 well pad facility (owned by QEP Energy Company). This existing equipment was previously carried within the applicable QEP Energy permit but to clarify ownership is being separated out into its own permit.

QEP Energy (QEPE) equipment separates and processes the production from all of the producing natural gas wells associated with this pad facility. The well production leaves the applicable QEPE equipment, is commingled into a single process stream and routed to a QEPM Gathering I, LLC (QEPM) high-pressure separator (known as the dehydration unit separator).

In the dehydration unit separator, the fluids are separated into individual components (natural gas, produced water, hydrocarbon liquid). The hydrocarbon liquid (condensate) and produced water flow directly into their respective pipelines where they are sent to a Central Gathering Facility for further processing. The natural gas phase exits the dehydration unit separator and is sent to a tri-ethylene glycol (TEG) dehydration unit.

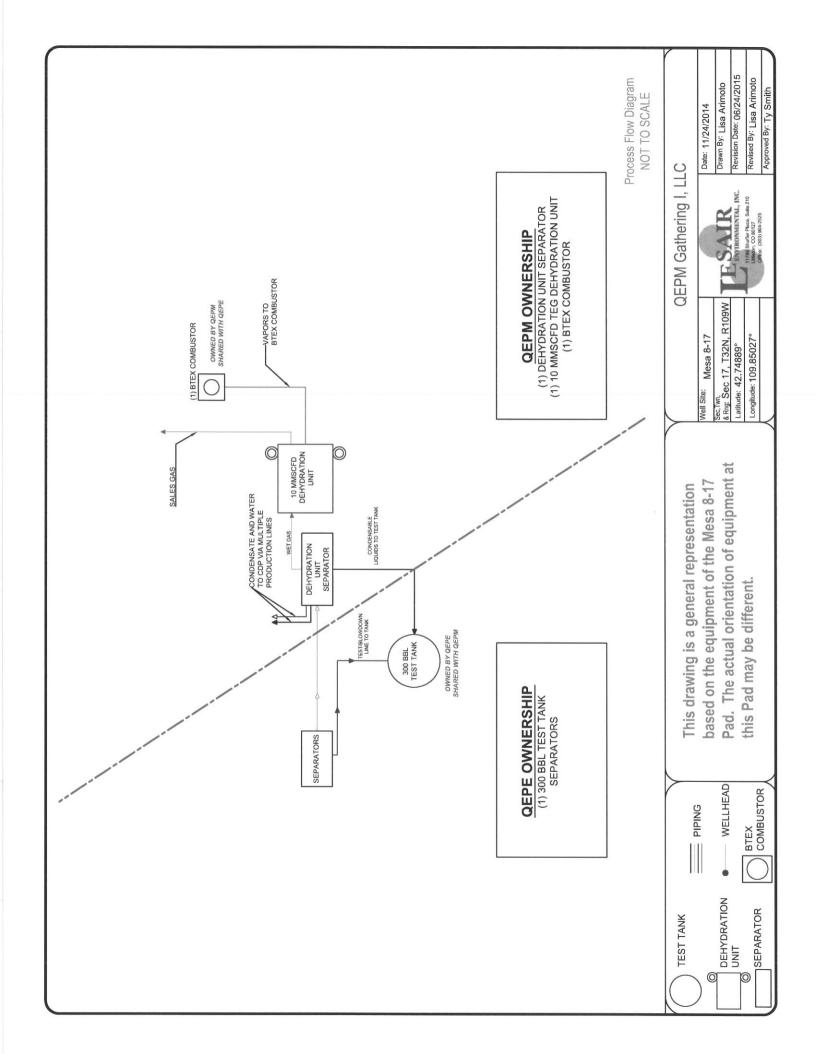
A 10 MMSCFD TEG dehydration unit (equipped with a 9015 PV Kimray glycol circulation pump, reboiler condenser and BTEX combustor) dehydrates the gas to meet a certain pipeline specification. Here the gas stream bubbles up through tri-ethylene glycol (TEG) in a process vessel known as a contactor. During this process water vapor is removed from the gas to meet a concentration determined by a sales contract. The pipeline quality natural gas exits the contactor, is measured, and then enters the gas gathering pipeline system.

The TEG is regenerated using heat in a vessel known as the glycol reboiler. The TEG is heated to a set temperature that boils the impurities out of the TEG, sending the vapors through a condenser to (1) one BTEX combustor where they are burned. (The BTEX combustor is owned by QEPM but is a shared control device also used by some of the QEPE processes onsite). The regenerated TEG is then circulated back through the contactor.

The liquids from the condenser are recovered in a blowcase pot. Pressurized gas is used to force all these recovered condensable liquids out of the blowcase pot to a 300 bbl. test tank (owned by QEPE but shared by QEPM). This is a closed system and any residual gas used in this process is routed to the BTEX combustor.

Fugitive emissions associated with the piping connections, flanges, valves, etc. occur due to the potential seeping of vapor from connections, seats, and seals.

Pneumatic controllers, operated using natural gas, are used to actuate level control valves on the separators.



Company Name: QEPM Gathering I, LLC Pinedale Field Mesa 8-17 Facility Name: Field Name:

Wyoming Air Quality Application Emission Summary Sheet

Uncontrolled Production Equipment Emissions

					ľ					Į.				
			Ž	NOX	00	0	202	72	Particu	lates	VOC	S	Total H	HAPS
Ref No.	Equipment	Note	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY
001	(1) 10 MMSCFD TEG Dehydration Unit	ø	00.0	00.00	00.00	0.00	0.00	00.00	0.00	0.00	4.90	21.48	3.61	15.80
002	(1) Flash Tank Separator(s)	q	00.0	00.0	00.0	0.00	00.0	00.0	00.00	0.00	1.86	8.15	0.16	0.70
003	(1) 0.125 MMBtu/hr TEG Reboiler	O	0.01	90.0	0.01	0.05	0.00	00.00	00.00	0.00	0.00	00.00	00.00	00.00
004	Fugitives	р	00.0	00.00	00.0	00.00	0.00	00.00	0.00	0.00	0.33	1.43	0.01	0.05
900	Pneumatic Controllers	ө	00.0	00.00	00.0	0.00	00.00	00.00	00.00	00.00	0.00	0.01	00.00	00.00
900	(1) 300 bbl Test Tank	Ţ	00.00	0.00	00.00	00.00	00.00	0.00	0.00	0.00	insig.	insig.	insig.	insig.
	Total		0.01	90.0	0.01	0.05	0.00	00.0	00.0	0.00	7.09	31.07	3.78	16.55

NOTES: a - Reboiler still column vent emissions calculated using GRL-GLYCalc 4.0 software, a Mesa 8-17 Pad Wet Gas Analysis, the maximum glycol circulation rate and the

current average estimated natural gas production rate.

b - TEG flash tank vapors are sent to BTEX combustor, however as a worst case scenario 100% of TEG flash tank vapors are being vented to atmosphere.

c - Burner emissions based on EPA AP-42 emission factors from Section 1.4, Tables 1.4-1 and 1.4-2 for uncontrolled natural gas burners (July 1998), the worst case assumption that burners operate 8,760 hours per year and a fuel heating value of 1079.7 Btu/SCF.

d - Fugitive emissions account for VOC/HAP vapors from connections, valves, tank hatches and relief ventivalves. Emission factors derived from table 2-4, PA-453/R-95-017

e - Pneumatic Controller VOC/HAP emissions based on VOC/HAP fraction of the instrument gas; consumption rates taken from manufacturer literature for specific sources.

f - Based on previous Promax and EPA Tanks process simulations as well as stack emission tests performed by QEP Energy, required by the WAQD, test tank emissions are

considered insignificant.

Company Name: QEPM Gathering I, LLC
Field Name: Pinedale Field
Facility Name: Mesa 8-17

Wyoming Air Quality Application Emission Summary Sheet

Controlled Production Equipment Emissions

		2												
			NOX	×	00		802	2	Particulates	lates	VOC	S	Total HAPs	IAPs
Ref No.	Equipment	Note	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY
001	(1) 10 MMSCFD TEG Dehydration Unit	В	0.00	0.01	00.00	0.00	0.00	0.00	0.00	0.00	0.01	0.03	0.00	0.01
002	(1) Flash Tank Separator(s)	q	0.05	0.20	0.01	0.05	00.00	0.00	00.00	00.00	0.04	0.16	00.00	0.01
003	(1) 0.125 MMBtu/hr TEG Reboiler	ပ	0.01	90.0	0.01	0.05	0.00	0.00	00.00	0.00	0.00	0.00	0.00	00.0
004	Fugitives	Б	0.00	0.00	0.00	00.00	0.00	0.00	00.00	0.00	insig.	insig.	insig.	insig.
900	Pneumatic Controllers	ө	0.00	0.00	00.00	00.00	0.00	0.00	00.00	0.00	0.00	0.01	0.00	00.0
900	(1) 300 bbl Test Tank	ţ	0.00	0.00	0.00	00.00	0.00	0.00	00.00	0.00	insig.	insig.	insig.	insig.
200	(1) BTEX Combustor	g	0.00	0.02	00.00	0.00	0.00	0.00	0.00	00.0	0.00	0.01	0.00	00.00
	Total		90.0	0.28	0.02	0.10	00.00	00.0	0.00	0.00	0.05	0.22	0.01	0.03

NOTES: a - Reboiler still column vent emissions are based on a 98% VOC/HAP destruction efficiency for dehydration unit vapors and WAQD flare emission factors for other criteria pollutants.

b - Flash tank emissions are based on 98% destruction efficiency for flash tank vapors.

c - Burner emissions based on EPA AP-42 emission factors from Section 1.4, Tables 1.4-1 and 1.4-2 for uncontrolled natural gas burners (July 1998), the worst case assumption

that burners operate 8,760 hours per year and a fuel heating value of 1079.7 Btu/SCF.

 d - Due to implementation of infrared LDAR program, both baseline and current fugitive emissions are being treated as insignificant (as approved by the WAQD)
 e - Pneumatic Controller VOC/HAP emissions based on VOC/HAP fraction of the instrument gas; consumption rates taken from manufacturer literature for specific sources.
 f - Based on previous Promax and EPA Tanks process simulations as well as stack emission tests performed by QEP Energy, required by the WAQD, test tank emissions are considered insignificant.

g - Combustor emissions are for combustor pilots only, other emissions are accounted for at controlled emissions source. Emissions are based on WAQD flare emission factors for criteria pollutants

Company Name: QEPM Gathering I, LLC

Field Name:

Pinedale Field

Facility Name:

Mesa 8-17

Dehydrator Still Column Vent Emission Calculations

GRI GLYCalc 4.0 Method

UNCONTROLLED EMISSIONS (As Per WAQD Methodology)

Annual Rate:

MMSCFD 8.0

gpm

For the 10 MMSCFD Unit

Glycol Pump Type: (1) Kimray 9015 PV
Pump Rate(s): 1.5

				Indiv	idual H	AP Com	ponent	Emiss	ions				
Reference No.		Benz	ene	Tolu	iene	Ethyl-B	enzene	Xyl	ene	n-He	xane	1000	2,4- /lpentane
		(Lb/Hr)	(TPY)	(Lb/Hr)	(TPY)	(Lb/Hr)	(TPY)	(Lb/Hr)	(TPY)	(Lb/Hr)	(TPY)	(Lb/Hr)	(TPY)
001	Reboiler	1.11	4.88	1.95	8.54	0.00	0.00	0.49	2.15	0.05	0.21	0.01	0.02
002	Flash Tank	0.04	0.19	0.04	0.19	0.00	0.00	0.00	0.02	0.06	0.28	0.01	0.03
	Total	1.16	5.07	1.99	8.73	0.00	0.00	0.49	2.17	0.11	0.49	0.01	0.05

Reference	Д	ggregated	Emissio	ons	
No.		Total I	HAP	VO	C
		(Lb/Hr)	(TPY)	(Lb/Hr)	(TPY)
001	Reboiler	3.61	15.80	4.90	21.48
002	Flash Tank	0.16	0.70	1.86	8.15
	Total	3.77	16.50	6.76	29.63

CONTROLLED EMISSIONS

8.0

MMSCFD

For the 10 MMSCFD Unit

Annual Rate: 8.0
Glycol Pump Type: (1) Kimray 9015 PV

Pump Rate(s): gpm

				Indivi	dual HA	AP Com	ponent	Emissi	ions				
Reference No.		Benz	ene	Tolu	ene	Ethyl-B	enzene	Xyl	ene	n-He	xane	THE REST 100000	2,4- Ipentane
		(Lb/Hr)	(TPY)	(Lb/Hr)	(TPY)	(Lb/Hr)	(TPY)	(Lb/Hr)	(TPY)	(Lb/Hr)	(TPY)	(Lb/Hr)	(TPY)
001	Reboiler	0.00	0.01	0.00	0.01	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
002	Flash Tank	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.01	0.00	0.00
	Total	0.00	0.01	0.00	0.01	0.00	0.00	0.00	0.00	0.00	0.01	0.00	0.00

Reference	A	ggregated l	Emissio	ons	
No.		Total I	HAP	VO	С
		(Lb/Hr)	(TPY)	(Lb/Hr)	(TPY)
001	Reboiler	0.00	0.01	0.01	0.03
002	Flash Tank	0.00	0.01	0.04	0.16
	Total	0.01	0.03	0.04	0.20

GRI-GLYCalc VERSION 4.0 - SUMMARY OF INPUT VALUES

Case Name: Mesa 8-17 Pad (2015 App)

File Name: L:\Datafile\GlyCalc 4.0 Data Files\QEPM\Wyoming\Mesa 8-17 Pad (2015 App)

lta.ddf

Date: June 30, 2015

DESCRIPTION:

Description: QEPM Gathering I, LLC- Pinedale

Mesa 8-17 Pad Wet Gas Analysis

Press/Temp/Dew Pt= 479/79/5.0 lbs/MMSCF

(1) Kimray 9015 PV Pumps @ 1.5gpm

Annual Rate of 8 MMSCFD

Annual Hours of Operation: 8760.0 hours/yr

WET GAS:

Temperature: 79.00 deg. F Pressure: 479.00 psig

Wet Gas Water Content: Saturated

Component	Conc. (vol %)
Carbon Dioxide	0.4798
Nitrogen	0.1206
Methane	92.8579
Ethane	4.5262
Propane	1.1036
Isobutane	0.2888
n-Butane	0.2591
Isopentane	0.1192
n-Pentane	0.0722
n-Hexane	0.0276
Cyclohexane Other Hexanes Heptanes Methylcyclohexane 2,2,4-Trimethylpentane	0.0160 0.0543 0.0291 0.0184 0.0022
Benzene	0.0097
Toluene	0.0093
Xylenes	0.0011
C8+ Heavies	0.0049

DRY GAS:

Flow Rate: 8.0 MMSCF/day Water Content: 5.0 lbs. H2O/MMSCF

LEAN GLYCOL:

Glycol Type: TEG
Water Content: 1.5 wt% H2O
Flow Rate: 1.5 gpm

Page: 2 PUMP:

Glycol Pump Type: Gas Injection Gas Injection Pump Volume Ratio: 0.080 acfm gas/gpm glycol

FLASH TANK:

Flash Control: Combustion device Flash Control Efficiency: 98.00 $\mbox{\%}$

Temperature: 100.0 deg. F
Pressure: 35.0 psig

REGENERATOR OVERHEADS CONTROL DEVICE:

Control Device: Condenser

Temperature: 95.0 deg. F Pressure: 12.0 psia

Control Device: Combustion Device

Destruction Efficiency: 98.0 %
Excess Oxygen: 5.0 %
Ambient Air Temperature: 50.0 deg. F

GRI-GLYCalc VERSION 4.0 - EMISSIONS SUMMARY

Case Name: Mesa 8-17 Pad (2015 App)
File Name: L:\Datafile\GlyCalc 4.0 Data Files\QEPM\Wyoming\Mesa 8-17 Pad (2015 App)

lta.ddf

Date: June 30, 2015

CONTROLLED REGENERATOR EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Methane	0.0027	0.066	0.0120
Ethane	0.0012	0.030	0.0054
Propane	0.0011	0.027	0.0049
Isobutane	0.0006	0.016	0.0028
n-Butane	0.0008	0.019	0.0034
Isopentane	0.0003	0.008	0.0014
n-Pentane	0.0003	0.008	0.0014
n-Hexane	0.0001	0.004	0.0007
Cyclohexane	0.0004	0.010	0.0018
Other Hexanes	0.0003	0.006	0.0011
Heptanes	0.0002	0.005	0.0008
Methylcyclohexane	0.0004	0.009	0.0016
2,2,4-Trimethylpentane	<0.0001	<0.001	<0.0001
Benzene	0.0019	0.046	0.0084
Toluene	0.0012	0.028	0.0051
Xylenes	0.0001	0.002	0.0003
C8+ Heavies	<0.0001	<0.001	<0.0001
Total Emissions	0.0117	0.281	0.0513
Total Hydrocarbon Emissions	0.0117	0.281	0.0513
Total VOC Emissions	0.0077	0.185	0.0338
Total HAP Emissions	0.0033	0.079	0.0145
Total BTEX Emissions	0.0032	0.076	0.0138

UNCONTROLLED REGENERATOR EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Methane	0.1383	3.319	0.6057
Ethane	0.0640	1.536	0.2804
Propane	0.0672	1.613	0.2943
Isobutane	0.0458	1.099	0.2005
n-Butane	0.0647	1.552	0.2833
Isopentane	0.0468	1.123	0.2049
n-Pentane	0.0415	0.995	0.1816
n-Hexane	0.0490	1.175	0.2145
Cyclohexane	0.1867	4.480	0.8177
Other Hexanes	0.0621	1.490	0.2719
Heptanes	0.1701	4.083	0.7451
Methylcyclohexane	0.3313	7.952	1.4512
2,2,4-Trimethylpentane	0.0050	0.120	0.0219
Benzene	1.1141	26.738	4.8797
Toluene	1.9487	46.770	8.5355
Xylenes	0.4907	11.776	2.1492
C8+ Heavies	0.2801	6.723	1.2269
Total Emissions	5.1060	122.543	22.3641

				Page: 2
Total Hydrocarbon	Emissions	5.1060	122.543	22.3641
Total VOC	Emissions	4.9037	117.688	21.4781
Total HAP	Emissions	3.6075	86.579	15.8007
Total BTEX	Emissions	3.5535	85.284	15.5643

FLASH GAS EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Methane	0.2204	5.289	0.9652
Ethane	0.0261	0.626	0.1142
Propane	0.0117	0.281	0.0513
Isobutane	0.0049	0.117	0.0214
n-Butane	0.0051	0.122	0.0223
Isopentane	0.0030	0.073	0.0133
n-Pentane	0.0021	0.051	0.0092
n-Hexane	0.0013	0.030	0.0055
Cyclohexane	0.0012	0.029	0.0053
Other Hexanes	0.0022	0.052	0.0095
Heptanes	0.0020	0.047	0.0086
Methylcyclohexane	0.0016	0.037	0.0068
2,2,4-Trimethylpentane	0.0001	0.003	0.0005
Benzene	0.0009	0.021	0.0038
Toluene	0.0009	0.021	0.0039
Xylenes C8+ Heavies	0.0001	0.002	0.0003 0.0013
Total Emissions	0.2836	6.808	1.2424
Total Hydrocarbon Emissions	0.2836	6.808	1.2424
Total VOC Emissions	0.0372	0.893	0.1629
Total HAP Emissions	0.0032	0.077	0.0140
Total BTEX Emissions	0.0018	0.044	0.0080

FLASH TANK OFF GAS

Component	lbs/hr	lbs/day	tons/yr
Methane Ethane Propane Isobutane		264.450 31.286 14.049 5.864	48.2621 5.7098 2.5639 1.0701
Isopentane n-Pentane n-Hexane Cyclohexane Other Hexanes	0.1054 0.0630 0.0601	1.513 1.442	0.4615 0.2761 0.2631
Heptanes Methylcyclohexane 2,2,4-Trimethylpentane Benzene Toluene	0.0778	0.144 1.031	0.3407 0.0262 0.1881
Xylenes C8+ Heavies	0.0040 0.0144		
Total Emissions	14.1825	340.379	62.1191
Total Hydrocarbon Emissions Total VOC Emissions			

Total HAP Emissions 0.1603 3.847 0.7021
Total BTEX Emissions 0.0913 2.190 0.3997

GRI-GLYCalc VERSION 4.0

Case Name: Mesa 8-17 Pad (2015 App)

File Name: L:\Datafile\GlyCalc 4.0 Data Files\QEPM\Wyoming\Mesa 8-17 Pad (2015 App)

lta.ddf

Date: June 30, 2015

ABSORBER

NOTE: Because the Calculated Absorber Stages was below the minimum allowed, GRI-GLYCalc has set the number of Absorber Stages to 1.25

and has calculated a revised Dry Gas Dew Point.

Calculated Absorber Stages: 1.25

2.76 lbs. H2O/MMSCF Calculated Dry Gas Dew Point:

> Temperature: 79.0 L. 479.0 psig 79.0 deg. F Pressure: 8.0000 MMSCF/day Dry Gas Flow Rate:

Glycol Losses with Dry Gas: 0.0164 lb/hr

Wet Gas Water Content: Saturated

Calculated Wet Gas Water Content: 54.47 lbs. H2O/MMSCF Calculated Lean Glycol Recirc. Ratio: 5.22 qal/lb H20

Remaining Absorbed Component in Dry Gas in Glycol Water 5.05% 94.95% Carbon Dioxide 99.83% 0.17% Nitrogen 99.99% 0.01% Methane 99.99% 0.01% Carbon Dioxide 99.99% 0.01% Ethane 99.96% 0.04% 99.92% Propane 0.08% Isobutane 99.88% n-Butane 99.83% Isopentane 99.81% n-Pentane 99.75% 0.12% 0.17% 0.19% n-Pentane 99.75% 0.25% n-Hexane 99.54%
Cyclohexane 97.99%
Other Hexanes 99.66%
Heptanes 99.03%
Methylcyclohexane 97.50% 0.46% 2.01% 0.34% 0.97% 2.50% 2,2,4-Trimethylpentane 99.58% 0.42% Benzene 82.70%
Toluene 73.60%
Xylenes 51.86%
C8+ Heavies 96.06% 17.30% 26.40% 48.14% 96.06% 3.94%

GRI-GLYCalc VERSION 4.0 - STREAM REPORT

Case Name: Mesa 8-17 Pad (2015 App)

File Name: L:\Datafile\GlyCalc 4.0 Data Files\QEPM\Wyoming\Mesa 8-17 Pad (2015 App)

lta.ddf

Date: June 30, 2015

CONDENSER VENT STREAM

Temperature: 95.00 deg. F Pressure: 12.00 psia Flow Rate: 7.25e+000 scfh

Component		Loading (lb/hr)
Carbon Dioxide Nitrogen Methane	6.88e+000 8.18e+000 5.62e-002 4.48e+001 1.07e+001	6.88e-002 3.01e-004 1.37e-001
Isobutane n-Butane Isopentane	6.68e+000 2.91e+000 3.54e+000 1.17e+000	3.23e-002 3.93e-002 1.61e-002
Cyclohexane Other Hexanes	7.93e-001 4.93e-001	2.02e-002 1.31e-002 9.45e-003
Toluene	6.45e+000 3.30e+000 1.65e-001	9.63e-002 5.81e-002 3.34e-003
Total Components	100.00	6.78e-001

GRI-GLYCalc VERSION 4.0 - STREAM REPORT

Case Name: Mesa 8-17 Pad (2015 App)

File Name: L:\Datafile\GlyCalc 4.0 Data Files\QEPM\Wyoming\Mesa 8-17 Pad (2015 App)

lta.ddf

Date: June 30, 2015

REGENERATOR OVERHEADS STREAM

Temperature: 212.00 deg. F Pressure: 14.70 psia Flow Rate: 3.89e+002 scfh

Component	Conc. (vol%)	
Carbon Dioxide Nitrogen Methane	9.34e+001 1.58e-001 1.06e-003 8.41e-001 2.08e-001	7.15e-002 3.05e-004 1.38e-001
Isobutane n-Butane Isopentane	1.49e-001 7.68e-002 1.09e-001 6.32e-002 5.61e-002	4.58e-002 6.47e-002 4.68e-002
Cyclohexane Other Hexanes	7.02e-002 1.66e-001	1.87e-001 6.21e-002 1.70e-001
Toluene Xylenes C8+ Heavies	1.39e+000 2.06e+000 4.51e-001 1.60e-001	1.11e+000 1.95e+000 4.91e-001 2.80e-001
Toluene Xylenes	2.06e+000 4.51e-001 1.60e-001	1.95e+000 4.91e-001

GRI-GLYCalc VERSION 4.0 - STREAM REPORT

Case Name: Mesa 8-17 Pad (2015 App)

File Name: L:\Datafile\GlyCalc 4.0 Data Files\QEPM\Wyoming\Mesa 8-17 Pad (2015 App)

lta.ddf

Date: June 30, 2015

FLASH TANK OFF GAS STREAM

Temperature: 100.00 deg. F Pressure: 49.70 psia Flow Rate: 2.93e+002 scfh

Component		Loading (lb/hr)
Carbon Dioxide Nitrogen Methane	1.52e-001 1.14e+000 1.16e-001 8.90e+001 5.61e+000	3.88e-001 2.52e-002 1.10e+001
Isobutane n-Butane Isopentane	1.72e+000 5.44e-001 5.66e-001 2.72e-001 1.89e-001	2.44e-001 2.54e-001 1.52e-001
Cyclohexane Other Hexanes	1.63e-001 1.26e-001	6.01e-002 1.09e-001 9.79e-002
Toluene	7.12e-002 6.23e-002 4.87e-003	4.29e-002 4.43e-002 3.99e-003

Total Components 100.00 1.46e+001

QUESTAR APPLIED TECHNOLOGY

1210 D. Street, Rock Springs, Wyoming 82901 (307) 352-7292

LIMS ID:

N/A

Description:

Mesa 8-17 Pad

Analysis Date/Time: Analyst Initials:

6/13/2014 PRP 11:40 AM Field: ML#: Pinedale QEP

Analyst Initials: Instrument ID:

Instrument 1 QPC68.D GC Method:

Quesbtex

Data File: Date Sampled:

6/12/2014

Component	Mol9	6	W	′t%	LV%
Methane	92.8579		84.6256	89.0817	
Ethane	4.5262		7.7315	6.8696	
Propane	1.1036		2.7645	1.7221	
Isobutane	0.2888		0.9537	0.5351	
n-Butane	0.2591		0.8554	0.4626	
Neopentane	0.0115		0.0470	0.0249	
Isopentane	0.1077		0.4415	0.2233	
n-Pentane	0.0722		0.2960	0.1481	
2,2-Dimethylbutane	0.0044		0.0215	0.0104	
2,3-Dimethylbutane	0.0094		0.0462	0.0219	
2-Methylpentane	0.0252		0.1235	0.0593	
3-Methylpentane	0.0153		0.0749	0.0354	
n-Hexane	0.0276		0.1350	0.0642	
Heptanes	0.0847		0.4521	0.1866	
Octanes	0.0040		0.0260	0.0112	
Nonanes	0.0014		0.0092	0.0035	
Decanes plus	0.0006		0.0049	0.0021	
Nitrogen	0.1206		0.1920	0.0749	
Carbon Dioxide	0.4798		1.1995	0.4631	
Oxygen	0.0000		0.0000	0.0000	
Hydrogen Sulfide	0.0000		0.0000	0.0000	
Total	100.0000		100.0000	100.000	0
Global Properties		Units			
Gross BTU/Real CF	1084.8		BTU/SCF at	60°F and14.73 psia	
Sat.Gross BTU/Real CF	1067.1		BTU/SCF at	60°F and14.73 psia	
Gas Compressibility (Z)	0.9976				
Specific Gravity	0.6093		air=1		
Avg Molecular Weight	17.603		gm/mole		
Propane GPM	0.302456		gal/MCF		
Butane GPM	0.175741		gal/MCF		
Gasoline GPM	0.134692		gal/MCF		
26# Gasoline GPM	0.216167		gal/MCF		
Total GPM	1.918933		gal/MCF		
Base Mol%	99.485		%v/v		
Sample Temperature:	79		°F		
Sample Pressure:	479		psig		
H2SLength of Stain Tube	e N/A		ppm		

Component	Mol%	Wt%	LV%
Benzene	0.0097	0.0433	0.0154
Toluene	0.0093	0.0489	0.0177
Ethylbenzene	0.0000	0.0000	0.0000
M&P Xylene	0.0011	0.0067	0.0024
O-Xylene	0.0000	0.0000	0.0000
2,2,4-Trimethylpentane	0.0022	0.0144	0.0063
Cyclopentane	0.0000	0.0000	0.0000
Cyclohexane	0.0160	0.0767	0.0309
Methylcyclohexane	0.0184	0.1028	0.0420
Description:	Mesa 8-17 Pad		

GRI GlyCalc Information

Component	Mol%	Wt%	LV%
Carbon Dioxide	0.4798	1.1995	0.4631
Hydrogen Sulfide	0.0000	0.0000	0.0000
Nitrogen	0.1206	0.1920	0.0749
Methane	92.8579	84.6256	89.0817
Ethane	4.5262	7.7315	6.8696
Propane	1.1036	2.7645	1.7221
Isobutane	0.2888	0.9537	0.5351
n-Butane	0.2591	0.8554	0.4626
Isopentane	0.1192	0.4885	0.2482
n-Pentane	0.0722	0.2960	0.1481
Cyclopentane	0.0000	0.0000	0.0000
n-Hexane	0.0276	0.1350	0.0642
Cyclohexane	0.0160	0.0767	0.0309
Other Hexanes	0.0543	0.2661	0.1270
Heptanes	0.0291	0.1660	0.0743
Methylcyclohexane	0.0184	0.1028	0.0420
2,2,4 Trimethylpentane	0.0022	0.0144	0.0063
Benzene	0.0097	0.0433	0.0154
Toluene	0.0093	0.0489	0.0177
Ethylbenzene	0.0000	0.0000	0.0000
Xylenes	0.0011	0.0067	0.0024
C8+ Heavies	0.0049	0.0334	0.0144
Subtotal	100.0000	100.0000	100.0000
Oxygen	0.0000	0.0000	0.0000
Total	100.0000	100.0000	100.0000

Company Name: Facility Name: Field Name:

QEPM Gathering I, LLC Pinedale Field Mesa 8-17

Wyoming Air Quality Standards and Regulations

Enclosed Flare Emission Analysis Worksheet

(Based on Office of Air Quality Planning and Standards, EPA, AP-42 Manual, Fifth Edition, January 1995, Section 13.5)

Source with vapors sent to the Combustion Chamber	Vapor Volume (SCFD)	Vapor Heating Value (Btu/scf)	H2S Content (%)	NOx (lb/hr)	NOx (TPY)	CO (lb/hr) CO	/hr) CC	стРУ)	S02 (lb/hr)	SO2 (TPY)	VOC (Ib/hr)	VOC (TPY)	HAPs (lb/hr)	HAPs (TPY)
10MMSCFD Dehydration Unit 1	174	1841	0	00'0	0.01	0	0.00	0.00	00.0	00.00	0.01	0.03	0.00	0.01
Flash Tank Separator	7032	1102	0	0.05	0.20		0.01	0.05	0.00	00.00	0.04	0.16	00.00	0.01
Pilot Gas	009	1080	0	00.0	0.02		0.00	0.00	0.00	00.00	0.00	0.01	0.00	0.00
Total	7806		0	0.05	0.22		0.01	90.0	00.0	00.00	0.05	0.20	0.01	0.03
NOTES	MOTES: 4 Englosed flore MOV	A flore NO.		d onoionim h	o do booo	io i idi	2000	oion doite	aoiooiaa k	footors roate	and On aminainan hanned on continuous anotation union aminaina fortun sommatod has MDEO in OSO Braduation	2000 410	a distribution	

NOTES: 1 - Enclosed flare NOx and CO emissions based on continuous operation, using emission factors requested by WDEQ in O&G Production Facilities C6S2 Guidance, Appendix B13.

2 - Enclosed flare VOC emissions based on 98% destruction efficiency of the control equipment.

600	24	25
(SCFD)	(hrs/day)	(SCF/hr)
Pilot Gas		101 083

Condenser Conder	Condenser
Vent Gas	Vent Gas
(SCF/hr)	(SCFD)
7	174

vho	Flash Vent Gas (SCFD)	7032
10 MMSCED Deby	Flash Vent Gas (SCF/hr) (S	293
	Flas	

Company Name:

QEPM Gathering I, LLC

Field Name:

Pinedale Field Mesa 8-17

Facility Name:

Emission Calculation for External Combustion Sources

AP-42 Calculation Method

(For Estimating Emissions, Using Emission Factors from EPA AP-42, Table 1.4-1 and Table 1.4-2)

Burner Data

Reference No.	Burner Rating (MMBtu/Hr)	Count	Equipment	Annual Op Time (hours)	Fuel Type	Fuel Htg Value (Btu/scf)	Fraction of VOC ¹
003	0.125	1	TEG Reboiler(s)	8759	Field	1080	0.06

^{1 -} Fraction of VOC is derived from the fuel gas analysis (MW_{VOC}/MW_{TOTAL})

Reference	Consumption			Annual	Fuel	Fuel Htg	VOC
No.	Rating (Ft3/Hr)	Count	Equipment	Op Time (hours)	Type	Value (Btu/scf)	Fraction
	(1 (5/111)			(Hours)		(Blu/SCI)	_

^{1 -} Fraction of VOC is derived from the fuel gas analysis (MW_{VOC}/MW_{TOTAL})

Emission Factors

Reference	Burner			Emission	n Factors		
No.	Rating	NOx	CO	SO ₂	PM	TOC ²	VOC 3
	(MMBtu/Hr)	(Lb/MMFt ³)					
003	0.125	100.0	84.0	0.6	7.6	11.0	0.7
EF	Source	AP-42	AP-42	AP-42	AP-42	AP-42	Estimate

²⁻ Total Organic Compunds (TOC)

^{3 -} VOC emission factor determined by taking TOC factor times fraction of fuel gas that was VOC (as per C6S2 guidance, Mar 10).

Reference	Consumption			Emission	n Factors		
No.	Rating (Ft3/Hr)	NOx (Lb/MMFt ³)	CO (Lb/MMFt ³)	SO ₂ (Lb/MMFt ³)	PM (Lb/MMFt ³)	TOC (Lb/MMFt ³)	VOC (Lb/MMFt ³)
EF	Source	AP-42	AP-42	AP-42	AP-42	AP-42	Estimate

Emissions (Lb/Hr) = E.F. (Lb/MMft³) * FHV/1020 * Burner Rating (MMbtu/Hr) * $1/1020 * 1 \text{ MMft}³/1x10^6 \text{ ft}³ * 1x10^6 \text{ Btu/MMbtu}$ Emissions (TPY) = Emissions (Lb/Hr) * Annual Operating Time (Hr/Yr) * 1 ton/2,000 Lb

Source Emissions

Reference				5	Source Emi	ssions				
No.	NOx		С	0	S	O ₂	P	M	VC	C
	(Lb/Hr)	(TPY)	(Lb/Hr)	(TPY)	(Lb/Hr)	(TPY)	(Lb/Hr)	(TPY)	(Lb/Hr)	(TPY)
003	0.01	0.06	0.01	0.05	0.00	0.00	0.00	0.00	0.00	0.00
TOTAL	0.01	0.06	0.01	0.05	0.00	0.00	0.00	0.00	0.00	0.00

^{*} Thermo Electric Generator Emissions (Lb/Hr) = E.F. (Lb/MMft³) *Consumption Rate (ft³/Hr) * 1 MMft³/1x10⁶ ft³

QEPM Gathering I, LLC Company Name:

Field Name:

Pinedale Field Mesa 8-17 Facility Name:

Pneumatic Controller Equipment Emission Calculations

Current Controller Emissions (Uncontrolled)

Pneumatic Controller Emissions = (# of Controllers) * (Consumption Rate [scf/hr]) * (Ib-mole/379.41 scf) * motive gas molecular weight (Ib/lb-mole) * wt% VOC.

						VOC wt.	HAP wt.				
				Consumption		fraction of	fraction of	VOC	VOC	HAP	HAP
				Rate	Hours of	instrument	instrument	Emission		Emission	Emission
Component Description	Quantity	Manufacturer	Model	(scfh)	Operation	gas	gas	(lb/hr)	(TPY)	(lb/hr)	(TPY)
quid Level Controller(s)	4	Cemco/Wellmark	Mizer (low-bleed)	0.275	8760	90.0	0.0025	00.00	0.01	00.00	00.00
								00.0	0.01	00.00	00.0

NOTES: - There are two (2) liquid level controllers for each dehydration unit separator and two (2) for each flash tank. Consumption rate is typical, taken from Cemco/Wellmark Mizer manufacturer spec sheet at 6.6 scf/day. - Hours of operation for pneumatic controllers estimated at 24 hours per day, 7 days per week.

Current Controller Emissions (Controlled)

Pneumatic Controller Emissions = (# of Controllers) * (Consumption Rate [scf/hr]) * (Ib-mole/379.41 scf) * motive gas molecular weight (Ib/Ib-mole) * wt% VOC.

Company Name: QEPM Gathering I, LLC

Field Name:

Pinedale Field

Facility Name: Mesa 8-17

Fugitives Emission Calculation (LDAR)

Equipment Leak Emission Estimates for Oil and Gas Production Operations

(Emission Factors Derived From Table 2-4, EPA-453/R-95-017, "Protocol for Equipment Leak emission Estimates", November 1995)

		Equipment Se	rvice Categor	у
Component Type	Gas	Heavy Oil ¹ (<20 API Gravity) (lbs/hr/component)	Light Oil (>20 API Gravity) (lbs/hr/component)	Water/Light Oil 2
Connectors	4.41E-04	1.65E-05	4.63E-04	2.43E-04
Flanges	8.60E-04	8.60E-07	2.43E-04	6.39E-06
Open-ended Lines	4.41E-03	3.09E-04	3.09E-03	5.51E-04
Pumps 3	5.29E-03	7.05E-05	2.87E-02	5.29E-05
Valves 4	9.92E-03	1.85E-05	5.51E-03	2.16E-04
Other 5	1.94E-02	7.05E-05	1.65E-02	3.09E-02

^{* -} All factors are for total organic compound emission rates (includes non-VOC's such as methane and ethane).

- 2 Water/Light Oil factors apply to water streams in oil service with a water content greater than 50% to less than 99%. For streams with water content greater than 99%, the emission rate is considered negligable.
- 3 Pneumatic pump emissions are accounted for separately with the pneumatic pump and dehydration unit emission calculations.
- 4 Includes Pressure relief valves
- 5 "Other" equipment types include, but are not limited to, hatches, site glasses, regulators and other instrumentation. dump arms, hatches, instruments, meters, polished rods and vents.

Facility Equipment Totals: [(1) Dehy Separator, (1) Test Tank, (1) Dehy w/ Combustor]

	Equipment Service Category											
Component Type	Gas	Heavy Oil (<20 API Gravity)	Light Oil (>20 API Gravity)	Water/Light Oil								
Connectors	866	0	71	68								
Flanges	36	0	4	2								
Open-ended Lines	0	0	0	0								
Pumps	0	0	0	0								
Valves	142	0	25	23								
Other	15	0	0	0								

NOTE: The number of individual components are based on an actual site-specific equipment count performed for the Mesa 3-20 Pad facility. Components are determined based on the number of well heads, single separators, double separators, dehydration units (with combustors) and tanks there are on location.

Sample Calculation:

TOC (TPY) = component quantity * component factor * 8,760 hr/yr * 1 ton/2,000 lb.s VOC (TPY) = TOC * VOC Fraction from gas analysis

		Equipment Se	rvice Category	1
Component Type	Gas (TPY of TOC)	Heavy Oil (<20 API Gravity) (TPY of TOC)	Light Oil (>20 API Gravity) (TPY of TOC)	Water/Light Oil
Connectors	1.672462	0.000000	0.143975	0.072229
Flanges	0.135574	0.000000	0.004249	0.000056
Open-ended Lines	0.000000	0.000000	0.000000	0.000000
Pumps	0.000000	0.000000	0.000000	0.000000
Valves	6.170342	0.000000	0.603515	0.021765
Other	1.274625	0.000000	0.000000	0.000000
TOTAL	9.253002	0.000000	0.751739	0.094050
Weight VOC Fraction *	0.06	0.00	1.00	1.0
Weight HAP Fraction *	0.002	0.00	0.033	0.03
TPY VOC	0.58	0.00	0.75	0.0
lb/hr VOC	0.13	0.00	0.17	0.0
TPY HAP	0.02	0.00	0.02	0.0
lb/hr HAP	0.01	0.00	0.01	0.0

NOTE: * Mesa 8-17 Pad Wet Gas Analysis Wet Gas Analysis (06/12/14).

Source	VOC	; 1	HAP 1						
Cource	(lb/hr)	(TPY)	(lb/hr)	(TPY)					
Fugitives	0.33	1.43	0.01	0.05					
Fugitives (LDAR)	insig.	insig.	insig.	insig.					

NOTES: 1) - Due to implementation of an infrared (IR) LDAR program, both baseline and current fugitive emissions are being treated as insignificant (as approved by the WAQD).

^{1 -} The emission factor for pumps was not derived in the actual protocol, the factor for "other" has been substituted for completeness.

Company Name: QEPM Gathering I, LLC

Pinedale Field Mesa 8-17

Field Name: Facility Name:

Wet Gas Analysis Calculation Sheet

Based on: Mesa 8-17 Pad Wet Gas Analysis

ide 0.4798 0.0048 44.01 ide 0.4798 0.0048 44.01 1fide 0.0000 0.0000 34.08 0.1206 0.0012 28.02 92.8579 0.9286 16.04 1 4.5262 0.0453 30.07 1.1036 0.010 44.09 0.2888 0.0029 58.12 0.2591 0.0029 58.12 e 0.1192 0.0012 72.15 ne 0.0172 0.0007 72.15 ne 0.0072 0.0007 72.15 ne 0.0076 0.0002 84.18 nes 0.0543 0.0005 86.18 xane 0.0184 0.0002 98.19 entane 0.0022 0.0001 114.22			F		i	BTIJ Content
Mole % Mole Frac. Lb/Lb mole MN 0.4798 0.0048 44.01 44.01 0.0000 0.0000 34.08 34.08 0.1206 0.0012 28.02 16.04 1 4.5262 0.0453 30.07 1 1 0.2888 0.0029 58.12 2 2 0.2591 0.0026 58.12 2 2 0.1192 0.0012 72.15 2 2 0.0722 0.0007 72.15 2 2 0.0720 0.0007 72.15 2 3 0.0072 0.0007 70.08 3 3 0.0276 0.0003 86.18 3 3 0.0543 0.0005 84.18 3 3 0.0241 0.0003 86.18 3 3 0.0251 0.0003 86.18 3 3 0.0251 0.0003 98.19 3 0.0022 0.000			0	BTU Content	BTI	ם כסווובווור
0.4798 0.0048 44.01 0.0000 0.0000 34.08 0.1206 0.0012 28.02 92.8579 0.9286 16.04 1 4.5262 0.0453 30.07 1 1.1036 0.0110 44.09 6.2581 0.2888 0.0029 58.12 6.02591 0.0722 0.0012 72.15 6.008 0.0722 0.0007 72.15 6.008 0.0000 0.0000 70.08 6.18 0.0160 0.0003 86.18 6.0054 0.0543 0.0005 84.18 6.0021 0.0291 0.0003 100.21 6.0021 0.0184 0.0002 98.19 6.0002 0.0022 0.0000 114.22 6.0002	Lb/Lb mole	VOC HAP	Btu/scf	Btu/scf*Mole Frac	Btu/scf	Btu/scf*Mole Frac
0.0000 0.0000 34.08 0.1206 0.0012 28.02 92.8579 0.9286 16.04 1 4.5262 0.0453 30.07 1.1036 0.0110 44.09 0.2888 0.0029 58.12 0.2591 0.0026 58.12 0.0722 0.0007 72.15 0.0000 0.0000 70.08 0.0276 0.0003 86.18 0.0160 0.0003 86.18 0.0543 0.0005 84.18 0.0243 0.0003 100.21 0.0184 0.0003 100.21 0.0022 0.0000 114.22			0.0	00'0	0.0	00:0
0.1206 0.0012 28.02 92.8579 0.9286 16.04 1 4.5262 0.0453 30.07 1.1036 0.0110 44.09 0.2888 0.0029 58.12 0.2591 0.0026 58.12 0.01192 0.0007 72.15 0.00722 0.0007 72.15 0.0000 0.0000 70.08 0.0276 0.0003 86.18 0.0160 0.0003 84.18 0.0543 0.0003 100.21 0.0184 0.0003 10.21 0.0022 0.0000 114.22 0.0022 0.0000 114.22			586.8	00.0	637.1	00:0
92.8579 0.9286 16.04 1 4.5262 0.0453 30.07 1.1036 0.0110 44.09 0.2888 0.0029 58.12 0.2591 0.0026 58.12 0.01192 0.00012 72.15 0.0000 0.0000 70.08 0.0276 0.0003 86.18 0.0160 0.0003 84.18 0.0543 0.0005 84.18 0.0291 0.0003 100.21 0.0184 0.0003 98.19 0.0022 0.0000 114.22			0.0	00.0	0.0	00.00
4.5262 0.0453 30.07 1.1036 0.0110 44.09 0.2888 0.0029 58.12 0.2591 0.0026 58.12 0.01192 0.0012 72.15 0.0072 0.0007 72.15 0.0000 0.0000 70.08 0.0276 0.0003 86.18 0.0160 0.0003 84.18 0.0543 0.0005 86.18 0.0543 0.0003 100.21 0.0184 0.0002 98.19 0.0022 0.0000 114.22			909.4	844.45	1010.0	937.86
1.1036 0.0110 44.09 0.2888 0.0029 58.12 0.2591 0.0026 58.12 0.1192 0.0012 72.15 0.0722 0.0007 72.15 0.0276 0.0000 70.08 0.0276 0.0003 86.18 0.0543 0.0005 84.18 0.0543 0.0005 86.18 0.0184 0.0003 100.21 0.0184 0.0002 98.19 0.0022 0.0000 114.22			1618.7	73.27	1769.6	80.10
0.2888 0.0029 58.12 0.2591 0.0026 58.12 0.1192 0.0012 72.15 0.0722 0.0007 72.15 0.0000 0.0000 70.08 0.0276 0.0003 86.18 0.0160 0.0002 84.18 0.0543 0.0005 86.18 0.0291 0.0003 100.21 0.0184 0.0002 98.19 0.0022 0.0000 114.22		0.49	2314.9	25.55	2516.1	27.77
0.2591 0.0026 58.12 0.1192 0.0012 72.15 0.0722 0.0007 72.15 0.0000 0.0000 70.08 0.0276 0.0003 86.18 0.0160 0.0002 84.18 0.0543 0.0005 86.18 0.0291 0.0003 100.21 0.0184 0.0002 98.19 0.0022 0.0000 114.22		0.17	3000.4	8.67	3251.9	9.39
0.1192 0.0012 72.15 0.0722 0.0007 72.15 0.0000 0.0000 70.08 0.0276 0.0003 86.18 0.0160 0.0002 84.18 0.0543 0.0005 86.18 0.0291 0.0003 100.21 0.0184 0.0002 98.19 0.0022 0.0000 114.22 0.0027 0.0004 78.12		0.15	3010.8	7.80	3262.3	8.45
0.0722 0.0007 72.15 0.0000 0.0000 70.08 0.0276 0.0003 86.18 0.0160 0.0002 84.18 0.0543 0.0005 86.18 0.0291 0.0003 100.21 0.0184 0.0002 98.19 0.0022 0.0000 114.22 0.0022 0.0000 78.12		60.0	3699.0	4.41	4000.9	4.77
0.0000 0.0000 70.08 0.0276 0.0003 86.18 0.0160 0.0002 84.18 0.0543 0.0005 86.18 0.0291 0.0003 100.21 0.0184 0.0002 98.19 0.0022 0.0000 114.22		0.05	3706.9	2.68	4008.9	2.89
0.0276 0.0003 86.18 0.0160 0.0002 84.18 0.0543 0.0005 86.18 0.0291 0.0003 100.21 0.0184 0.0002 98.19 0.0022 0.0000 114.22		00.0	3512.2	00.00	3763.4	00.00
0.0160 0.0002 84.18 0.0543 0.0005 86.18 0.0291 0.0003 100.21 0.0184 0.0002 98.19 0.0022 0.0000 114.22		0.02 0.02	2 4404.1	1.22	4750.2	1.31
0.0543 0.0005 86.18 0.0291 0.0003 100.21 0.0184 0.0002 98.19 0.0022 0.0000 114.22		0.01	4179.9	0.67	4481.2	0.72
0.022 0.0000 114.22		0.05	4392.7	2.39	4744.5	2.58
0.0022 0.0000 114.22		0.03	5100.3	1.48	5500.4	1.60
0.0022 0.0000 114.22		0.02	4863.9	0.89	5215.7	96.0
11 A 70 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0		0.00 00.0	0 5779.1	0.13	6231.5	0.14
0.000.0	0.0001 78.11 0.01	0.01 0.01	1 3591.1	0.35	3741.5	0.36
Toluene 0.0093 0.0001 92.14 0.0		0.01 0.01	1 4273.7	0.40	4474.5	0.42
ne 0.0000 0.0000 106.17		0.00 00.00	0 4970.7	00.0	5221.7	0.00
Xylenes 0.00011 0.0000 106.17 0.0		0.00 0.00	0 4957.4	0.05	5208.4	0.06
315.00		0.02	5796.3	0.28	5794.1	0.28
Totals 100.0000 1.0000 17.610	17.6100	1.1096 0.0436	9	974.67		1079.66

Weight Fraction of Vapors that are VOC: Weight Fraction of Non-Methane Vapors that are VOC: Weight Fraction of Vapors that are HAP:

Gas Specific Gravity:

0.0630 0.4086 0.0025 0.6079

Lesair Environmental, Inc. www.lesair.com

Company Name:

QEPM Gathering I, LLC

Field Name:

Pinedale Field

Facility Name:

Mesa 8-17

Flare Gas Analysis Calculation Sheet

Based on: Glycalc 4.0: Mesa 8-17 post condenser gas composition

10 MMSCFD

							LHV	HHV						
						ВТ	U Content	ВТ	U Content					
Component	Mole %	Mole Frac.	Lb/Lb mole	MW	VOC	Btu/scf	Btu/scf*Mole Frac	Btu/scf	Btu/scf*Mole Frac					
H2O	6.88	0.0688				0.0	0.00	637.1	43.83					
Oxygen	0.00	0.0000	32.00	0.00		0.0	0.00	0.0	0.00					
CO2	7.13	0.0713	44.01	3.14		0.0	0.00	0.0	0.00					
N2	0.06	0.0006	28.02	0.02		0.0	0.00	0.0	0.00					
Methane	45.40	0.4540	16.04	7.28		909.4	412.87	1010.0	458.54					
Ethane	10.70	0.1070	30.07	3.22		1618.7	173.20	1769.6	189.35					
Propane	6.62	0.0662	44.09	2.92	2.92	2314.9	153.25	2516.1	166.57					
I-Butane	2.95	0.0295	58.12	1.71	1.71	3000.4	88.51	3251.9	95.93					
N-Butane	3.68	0.0368	58.12	2.14	2.14	3010.8	110.80	3262.3	120.05					
I-Pentane	1.51	0.0151	72.15	1.09	1.09	3699.0	55.85	4000.9	60.41					
N-Pentane	1.35	0.0135	72.15	0.97	0.97	3706.9	50.04	4008.9	54.12					
Hexane+	13.72	0.1372	125.74	17.25	17.25	4403.8	604.29	4755.9	652.61					
Totals	100.00	1.0000		39.7436	26.0898		1648.82		1841.41					

Fraction of Vapors that are VOC:

Fraction of Non-Methane Vapors that are VOC:

Fraction of Vapors that are H2S:

Gas Specific Gravity:

0.6565

0.8037

0.0000

1.3719

Based on: Glycalc 4.0: Mesa 8-17 flash tank off gas composition 10 MMSCFD

						ВТ	LHV U Content	ВТ	HHV U Content
Component	Mole %	Mole Frac.	Lb/Lb mole	MW	VOC	Btu/scf	Btu/scf*Mole Frac	Btu/scf	Btu/scf*Mole Frac
H2O	0.03	0.0003				0.0	0.00	637.1	0.22
Oxygen	0.00	0.0000	32.00	0.00		0.0	0.00	0.0	0.00
CO2	0.88	0.0088	44.01	0.39		0.0	0.00	0.0	0.00
N2	0.12	0.0012	28.02	0.03		0.0	0.00	0.0	0.00
Methane	90.70	0.9070	16.04	14.55		909.4	824.83	1010.0	916.07
Ethane	5.35	0.0535	30.07	1.61		1618.7	86.60	1769.6	94.67
Propane	1.48	0.0148	44.09	0.65	0.65	2314.9	34.26	2516.1	37.24
I-Butane	0.43	0.0043	58.12	0.25	0.25	3000.4	12.78	3251.9	13.85
N-Butane	0.41	0.0041	58.12	0.24	0.24	3010.8	12.37	3262.3	13.41
I-Pentane	0.19	0.0019	72.15	0.13	0.13	3699.0	6.92	4000.9	7.48
N-Pentane	0.12	0.0012	72.15	0.09	0.09	3706.9	4.49	4008.9	4.85
Hexane+	0.29	0.0029	125.74	0.37	0.37	4403.8	12.95	4755.9	13.98
Totals	100.00	1.0000		18.3077	1.7309		995.19		1101.77

Fraction of Vapors that are VOC:

0.0945

Fraction of Non-Methane Vapors that are VOC:

0.4604

Fraction of Vapors that are H2S:

0.0000

Gas Specific Gravity:

0.6320

Company Name: **QEPM Gathering I, LLC**

Facility Name: Mesa 8-17

Attachment C

Emissions Comparison and Offset Tracking Sheet

Company Name: QEPM Gathering I, LLC Facility Name: Mesa 8-17

Emissions Comparison (TPY)

Current Actual Emissions: Mesa 8-17 VOC 0.2 NOx 0.3 Historical Actual Emissions *: Mesa 8-17 VOC 7.3 NOx 4.7 Historical Actual Difference Pistorical VoC, 1.1:1 for Nox) VOC -7.1 NOx -4.4 Offset (1.5:1 for VOC, 1.1:1 for Nox) VOC 7.1 Credit NOx 4.4 Credit
--

_		_	_	_	_	_	_	_	_	_	_	_	_	_	_	_	_	_	_	_	_	_	_	_	_	_	_	_	_	_	_	_	_	_	_	_	_	_
Т	Reason for Change		Replacement of uncontrolled IR 12-5VGA 660 hp engine with Waukesha H24GSI 483 hp engine with AFRC and NSCR	Installation of turbine	Routing condensate to sales line instead of truck loadout	Increase VOC emission limit for four engines	Route all condensate through ST-3.	Establish QEPM baseline and current emissions resulting from QEPM and QEPE permit split	Establish QEPM baseline and current emissions resulting from QEPM and QEPE permit split	Establish QEPM baseline and current emissions resulting from QEPM and QEPE permit split	Establish QEPM baseline and current emissions resulting from QEPM and QEPE permit split	Establish QEPM baseline and current emissions resulting from QEPM and QEPE permit split	Establish QEPM baseline and current emissions resulting from QEPM and QEPE permit split	Establish QEPM baseline and current emissions resulting from QEPM and QEPE permit split	Establish QEPM baseline and current emissions resulting from QEPM and QEPE permit split	Establish QEPM baseline and current emissions resulting from QEPM and QEPE permit split	Establish QEPM baseline and current emissions resulting from QEPM and QEPE permit split	Establish QEPM baseline and current emissions resulting from QEPM and QEPE permit split	Establish QEPM baseline and current emissions resulting from QEPM and QEPE permit split	Establish QEPM baseline and current emissions resulting from QEPM and QEPE permit split	Establish QEPM baseline and current emissions resulting from QEPM and QEPE permit split	Establish QEPM baseline and current emissions resulting from QEPM and QEPE permit split	Establish QEPM baseline and current emissions resulting from QEPM and QEPE permit split	Establish QEPM baseline and current emissions resulting from QEPM and QEPE permit split	Establish QEPM baseline and current emissions resulting from QEPM and QEPE permit split	Establish QEPM baseline and current emissions resulting from QEPM and QEPE permit split	Establish QEPM baseline and current emissions resulting from QEPM and QEPE permit split	Establish QEPM baseline and current emissions resulting from QEPM and QEPE permit split	Establish QEPM baseline and current emissions resulting from QEPM and QEPE permit split	Establish QEPM baseline and current emissions resulting from QEPM and QEPE permit split	Establish QEPM baseline and current emissions resulting from QEPM and QEPE permit split	Establish QEPM baseline and current emissions resulting from QEPM and QEPE permit split	Establish QEPM baseline and current emissions resulting from QEPM and QEPE permit split	Establish QEPM baseline and current emissions resulting from QEPM and QEPE permit split	Establish QEPM baseline and current emissions resulting from QEPM and QEPE permit split	Establish QEPM baseline and current emissions resulting from Mesa 8-17 Dehy Swap with Mesa 13-5		
SUBLETTE COUNTY PERMITTED EMISSIONS April 1, 2008 - PRESENT	NOx Offset Bank		-98.0	-0.7	0.0	0.0	0.3	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	4.4		-102.8
, 2008 -	VOC Offset Bank		-21.0	-10.5	4.7	34.4	1.7	0.0	0.0	0.0	0.0	0.0	0,0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	-7.1		-7.3
April 1	increase/decrease from baseline emissions (TPY)	NOx	-98.0	-0.7	0.0	0.0	0.3	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	-4.4		-102.8
ISSIONS	increase/de baseline emi	voc	-21.0	-10.5	-4.7	22.9	1.1	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	-7.1		-19.3
TED EM	Baseline Emissions (TPY)	NOx	100.3	139.5	139.2	139.5	0.0	2.6	2.4	2.8	0.7	1.6	6.0	0.1	9.0	9.1	2.7	4.7	2.5	9.1	2.7	6.4	0.7	1.7	0.5	2.9	0.1	0.5	5.9		0.1	2.0	2.8	2.7	1.6	4.7		9.695
RMIT		VOC	24.3	128.4	113.0	114.1	0.0	9.1	1.5	3.2	0.5	1.0	0.5	9.9	0.4	1.3	1.8	7.3	1.7	2.4	3.6	1.8	2.1	2.3	1.7	3.4	10.8	2.0	4.8		9.1	4.1	5.7	6.4	2.7	7.3		477.4
UNTY PE	Equipment Design / Current Actual Emissions (TPY)	NOx	2.3	138.8	139.2	139.5	0.3	2.6	2.4	2.8	0.7	9.1	6.0	0.1	9.0	9.1	2.7	4.7	2.5	9.1	2.7	0.4	0.7	1.7	0.5	2.9	0.1	0.5	2.9		0.1	2.0	2.8	2.7	1.6	0.3		466.8
TTE CO	Equipment Do Actual Emi	VOC	3.3	117.9	108.3	137.0	1.1	9.1	1.5	3.2	0.5	1.0	0.5	9'9	0.4	1.3	1.8	7.3	1.7	2.4	3.6	8.1	2.1	2.3	1.7	3.4	10.8	2.0	4.8		9.1	4.1	5.7	6.4	2.7	0.2		458.1
SUBLE	permit/waiver / AP#		MD-15150	MD-7332	MD-8682	MD-11378	MD-10895																															
	date of receipt (permit)		10/7/2013	7/31/2008	7/16/2010	3/2/2011	10/22/2010																															
	date of permit application		6/17/2013	2/8/2008	3/31/2010	11/11/2010	6/30/2010	12/1/2014	12/1/2014	12/1/2014	12/1/2014	12/1/2014	12/1/2014	12/1/2014	12/1/2014	12/1/2014	12/1/2014	12/1/2014	12/1/2014	12/1/2014	12/1/2014	12/1/2014	12/1/2014	12/1/2014	12/1/2014	12/1/2014	12/1/2014	12/1/2014	12/1/2014	12/1/2014	12/1/2014	12/1/2014	12/1/2014	12/1/2014	12/1/2014	7/7/2015		
	facility		Dry Piney Compressor Station	Pinedale Complex	Pinedale Complex	Pinedale Complex - Gobblers Knob	Pinedale Complex - Stab Plant	Mesa 6-16 Pad	Mesa 5-8 Pad	Mesa 9-8 Pad	Mesa 12-8 Pad	Mesa 12-16 Pad	Mesa 13-16 Pad	Pinedale Unit 8 Well	Mesa 3-21 Pad	Mesa 15-9 Pad	Mesa 9-16 Pad	Mesa 8-17 Pad	Mesa 11-7 Pad	Mesa 15-16 Pad	Stewart Point 5-20 Pad	Mesa 14-16 Pad	Mesa 15-6 Pad	Mesa 10-16 Pad	Stewart Point 1-30 Pad	Mesa 6-7 Pad	Mesa Unit 13-05V Well	Mesa 1 Pad	Mesa 7-7 Pad	Mesa 3-7 Pad	Mesa Unit 4-8 Well	Stewart Point 14-20 Pad	Stewart Point 7-20 Pad	Stewart Point 2-20 Pad	Mesa 11-16 Pad	Mesa 8-17 Pad		QEPM TOTAL
	field		Dry Piney	Pinedale	Pinedale	Pinedale	Pinedale	Pinedale	Pinedale	Pinedale	Pinedale	Pinedale	Pinedale	Pinedale	Pinedale	Pinedale	Pinedale	Pinedale	Pinedale	Pinedale	Pinedale	Pinedale	Pinedale	Pinedale	Pinedale	Pinedale	Pinedale	Pinedale	Pinedale	Pinedale	Pinedale	Pinedale	Pinedale	Pinedale	Pinedale	Pinedale		
	company		QEPM	QEPM	QEPM	QEPM	QEPM	QEPM	QEPM	QEPM	QEPM	QEPM	QEPM	QEPM	QEPM	QEPM	QEPM	QEPM	QEPM	QEPM	QEPM	QEPM	QEPM	QEPM	QEPM	QEPM	QEPM	QEPM	QEPM	QEPM	QEPM	QEPM	QEPM	QEPM	QEPM	QEPM		
	СОП		Ö	Ö	Ö	Ö	0	0	Ö	0	0	0	0	0	0	6	0	Ö	0	0	0	0	0	0	0	Ö	6	0	6	Ö	0	Ö	0	0	0	õ		